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IN THE CLAIMS:

1. (Previously Presented): A method comprising a multistep process for recovering one or more products from a solution containing one or more components selected from the group consisting of betaine, erythritol, inositol, sucrose, mannitol, glycerol, amino acids and mixtures thereof by using chromatographic separation comprising at least one step, where a weak acid cation exchange resin is used for the chromatographic separation.

2. (Original): The method of claim 1 wherein the solution to be treated is a sugar beet derived process solution.

3. (Original): The method of claim 2 wherein the sugar beet derived process solution is vinasse, molasses or betaine molasses.

4. (Original): The method of claim 1 wherein the product to be recovered is selected from the group consisting of betaine, erythritol, inositol, sucrose, mannitol, glycerol, amino acids and mixtures thereof.

5. (Original): The method of claim 1 wherein the product is betaine.

6. (Original): The method of claim 1 wherein the product is inositol.

7. (Original): The method of claim 1 wherein the product is mannitol.

8. (Previously Presented): The method of claim 1 wherein the chromatographic separation comprises at least one column or a part of a column, which contains a weak acid cation exchange resin.

9. (Previously Presented): The method of claim 1 wherein the chromatographic separation comprises at least one column or a part of a column, which contains a strong acid cation exchange resin.

10. (Previously Presented): The method of claim 1 wherein the weak acid cation exchange resin is an acrylic resin.

11. (Previously Presented): The method of claim 10 wherein the acrylic resin is derived from the group consisting of methyl acrylate, ethyl acrylate, butyl acrylate, methyl methacrylate, acrylonitrile, acrylic acids and mixtures thereof.

12. (Previously Presented): The method of claim 11 wherein the cation of said weak cation exchange resin is in the form selected from the group consisting of Na+, K+, H+, Mg2+ and Ca2+.

13. (Previously Presented): The method of claim 12 wherein the cation of said weak cation exchange resin is in Na+ and/or K+ form.

14. (Previously Presented): The method of claim 10 wherein the resin is crosslinked with divinyl benzene.

15. (Original): The method of claim 14 wherein the crosslinking degree of the resin is 3 to 8% by weight.

16. (Currently Amended): The method of ~~claims~~ claim 1 wherein the eluant used in the chromatographic separation is water.

17. (Previously Presented): The method of claim 1 comprising feeding the process solution to a first chromatographic column containing a weak acid cation exchange resin and then feeding a fraction from the first chromatographic column to a second chromatographic column containing a strong acid cation exchange resin.

18. (Previously Presented): The method of claim 1 comprising feeding the process solution to a first chromatographic column containing a strong acid cation exchange resin and then feeding a fraction from the first chromatographic column to a second chromatographic column containing a weak acid cation exchange resin.

19. (Currently Amended): The method of claim 18 comprising feeding a fraction from the second chromatographic column to a third chromatographic column containing a weak acid cation exchange resin and feeding a fraction from the third chromatographic column to a fourth chromatographic column containing a weak acid cation exchange resin.

20. (Previously Presented): The method of claim 17 wherein a concentration or filtration unit is arranged between said first and second chromatographic columns.

21. (Previously Presented): The method of claim 17 wherein, prior to feeding the fraction to a said second chromatographic column, said fraction is concentrated by evaporation.

22. (Previously Presented): The method of claim 18 wherein, prior to feeding the fraction to said second chromatographic column, said fraction is concentrated by evaporation.

23. (Currently Amended): The method of claim 19 wherein, prior to feeding the fraction to a further chromatographic column, said fraction is concentrated by evaporation.

24. (Previously Presented): The method of claim 20 wherein, prior to feeding the fraction from one chromatographic column to another, said fraction is concentrated by evaporation.

25. (Previously Presented): The method of claim 1 further comprising one or more of the steps of crystallization, ion exchange or precipitation.

26. (Original): The method of claim 1 wherein the temperature of the eluent used in the chromatographic separation is between 10°C and 95°C.

27. (Original) The method of claim 26 wherein the temperature of the eluent is between 65°C and 95°C.

28. (Previously Presented): The method of claim 1 wherein the particle size of the weak acid cation exchange resin is 10μm to 2000μm.

29. (Previously Presented): The method of claim 28 wherein the particle size of the weak acid cation exchange resin is 100μm to 400μm.

30. (Previously Presented): The method of claim 1 wherein a feed solution has a pH of from 6 to 11.

31. (Previously Presented): The method of claim 30 wherein the feed solution has a pH of from 9 to 11.

32. (Original): The method of claim 1 wherein the chromatographic separation is a batch process.

33. (Original): The method of claim 1 wherein the chromatographic separation is a simulated moving bed process.

34. (Original): The method of claim 33 wherein the simulated moving bed process is a sequential process.

35. (Original): The method of claim 33 wherein the simulated moving bed process is a continuous process.

36. (Previously Presented): The method of claim 34 where the weak acid cation exchange resin is used in at least one column.

37. (Previously Presented): The method of claim 35 where the weak acid cation exchange resin is used in at least one column.

38. (Previously Presented): The method of claim 34 wherein a strong acid cation exchange resin is used in at least one column.

39. (Previously Presented): The method of claim 35 where a strong acid cation exchange resin is used in at least one column.

40. (Original): The method of claim 1 comprising recovering betaine from a first and inositol, erythritol and mannitol from a second chromatographic column.

41. (Original): The method of claim 1 further comprising isolating betaine, inositol, erythritol, mannitol and glycerol by crystallization.

42. (Original): The method of claim 1 comprising recovering a sucrose fraction.

43. (Original): The method of claim 42 comprising separating amino acids and/or betaine from the sucrose fraction.

44. (Currently Amended): The method of claim 18 wherein a concentration or filtration unit is arranged between ~~the first and second~~ chromatographic columns.

45. (Previously Presented): The method of claim 19 wherein a concentration or filtration unit is arranged between chromatographic columns.